

FEDERAL UNIVERSITY OF TECHNOLOGY GOMBERA  
 MECHANICAL ENGINEERING DEPARTMENT  
 HARMATTAN SEMESTER EXAMINATION

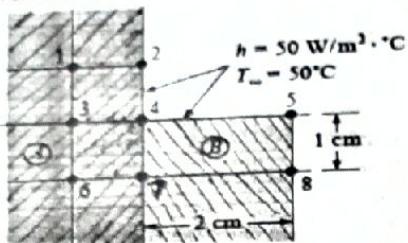
Course Title: Advanced Heat and Mass Transfer  
 Time Allowed: 3 hours

Course Code: MEE 413  
 Date: June 17, 2019

**Instruction:** Answer any **FIVE** questions. All questions carry equal marks.

**Question 1**

For the section shown in Figure 1, calculate the maximum time increment allowed for node 4 in a transient numerical environment. Also write the complete nodal equation for node 4.



	A	B	
$k$	20	2	$\text{W/m} \cdot ^\circ\text{C}$
$\rho$	7800	1600	$\text{kg/m}^3$
$c$	0.5	0.8	$\text{kJ/kg} \cdot ^\circ\text{C}$

Figure 1

**Question 2**

Calculate the steady-state temperatures for the nodes indicated in Figure 2.

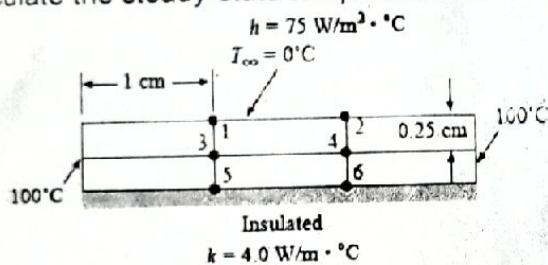


Figure 2

**Question 3**

Consider a steam pipe of length  $L = 20 \text{ m}$ , inner radius  $r_1 = 6 \text{ cm}$ , outer radius  $r_2 = 8 \text{ cm}$ , and thermal conductivity  $k = 20 \text{ W/m} \cdot \text{K}$ , as shown in Figure 3. The inner and outer surfaces of the pipe are maintained at average temperatures of  $T_1 = 150^\circ\text{C}$  and  $T_2 = 60^\circ\text{C}$ , respectively. Obtain a general relation for the temperature distribution inside the pipe under steady conditions and determine the rate of heat loss from the steam through the pipe.

**Question 4**

Consider a tube wall of inner and outer radii  $r_i$  and  $r_o$  whose temperatures are maintained at  $T_i$  and  $T_o$ , respectively. The thermal conductivity of the cylinder is temperature dependent and may be represented by an expression of the form  $k = k_0(1 + aT)$ , where  $k_0$  and  $a$  are constants. Obtain an expression for the heat transfer per unit length of the tube. What is the thermal resistance of the tube wall?

**Question 5**

A large block of steel [ $k = 45 \text{ W/mK}$ ,  $\alpha = 1.4 \times 10^{-5} \text{ m}^2/\text{s}$ ] is initially at a uniform temperature of  $35^\circ\text{C}$ . The surface is exposed to a heat flux (a) by suddenly raising the surface temperature to  $250^\circ\text{C}$  and (b) through a constant surface heat flux of  $3.2 \times 10^5 \text{ W/m}^2$ . Calculate the temperature at a depth of 2.5 cm after a time of 0.5 min for both these cases.

**Question 6**

Starting from first principle, derive the differential equation of heat conduction in the cylindrical coordinate.

Table A-1 | The error function.

$\frac{x}{2\sqrt{\alpha\tau}}$	$\text{erf} \frac{x}{2\sqrt{\alpha\tau}}$	$\frac{x}{2\sqrt{\alpha\tau}}$	$\text{erf} \frac{x}{2\sqrt{\alpha\tau}}$	$\frac{x}{2\sqrt{\alpha\tau}}$	$\text{erf} \frac{x}{2\sqrt{\alpha\tau}}$
0.00	0.00000	0.76	0.71754	1.52	0.96841
0.02	0.02256	0.78	0.73001	1.54	0.97059
0.04	0.04511	0.80	0.74210	1.56	0.97263
0.06	0.06762	0.82	0.75381	1.58	0.97455
0.08	0.09008	0.84	0.76514	1.60	0.97636
0.10	0.11246	0.86	0.77610	1.62	0.97804
0.12	0.13476	0.88	0.78669	1.64	0.97962
0.14	0.15695	0.90	0.79691	1.66	0.98110
0.16	0.17901	0.92	0.80677	1.68	0.98249
0.18	0.20094	0.94	0.81627	1.70	0.98379
0.20	0.22270	0.96	0.82542	1.72	0.98500
0.22	0.24430	0.98	0.83423	1.74	0.98613
0.24	0.26570	1.00	0.84270	1.76	0.98719
0.26	0.28690	1.02	0.85084	1.78	0.98817
0.28	0.30788	1.04	0.85865	1.80	0.98909
0.30	0.32863	1.06	0.86614	1.82	0.98994
0.32	0.34913	1.08	0.87333	1.84	0.99074
0.34	0.36936	1.10	0.88020	1.86	0.99147
0.36	0.38933	1.12	0.88709	1.88	0.99216
0.38	0.40901	1.14	0.89308	1.90	0.99279
0.40	0.42839	1.16	0.89910	1.92	0.99338
0.42	0.44749	1.18	0.90484	1.94	0.99392
0.44	0.46622	1.20	0.91031	1.96	0.99443
0.46	0.48466	1.22	0.91553	1.98	0.99489
0.48	0.50275	1.24	0.92050	2.00	0.995322
0.50	0.52050	1.26	0.92524	2.10	0.997020
0.52	0.53790	1.28	0.92973	2.20	0.998137
0.54	0.55494	1.30	0.93401	2.30	0.998857
0.56	0.57162	1.32	0.93806	2.40	0.999311
0.58	0.58792	1.34	0.94191	2.50	0.999593
0.60	0.60386	1.36	0.94556	2.60	0.999764
0.62	0.61941	1.38	0.94902	2.70	0.999866
0.64	0.63459	1.40	0.95228	2.80	0.999925
0.66	0.64938	1.42	0.95538	2.90	0.999959
0.68	0.66278	1.44	0.95830	3.00	0.999978
0.70	0.67780	1.46	0.96105	3.20	0.999994
0.72	0.69143	1.48	0.96365	3.40	0.999998
0.74	0.70468	1.50	0.96610	3.60	1.000000